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## The Leidenfrost Phenomenon

As given in the problem 3.1)

Integrating (i) with respect to z, we get

3.2) 
$$v\left(\frac{b}{2}\right) = 0 = \left(\frac{1}{2\eta}\frac{dP}{dr}\right)\cdot\left(\frac{b}{2}\right)^2 + C \qquad \dots$$
 (iii)

$$C = -\frac{b^2}{8n} \frac{dP}{dr}$$
 (0.5 point)

Note that C is not a real constant; its value depends on  $\frac{dP}{dr}$  which is a function of r.

3.3) Let Q be the volume rate of flow of the vapour through the cylindrical surface of  $2\pi rb$ .

$$\delta Q = v(z) \cdot 2\pi r \delta z$$
 where from (ii) and (iii): (0.3 point)

$$Q = 2 \int_{z=0}^{\frac{b}{2}} v(z) \cdot 2\pi r dz = \left(\frac{2\pi r}{\eta} \frac{dP}{dr}\right) \int_{z=0}^{\frac{b}{2}} \left[z^2 - \frac{b^2}{4}\right] dz$$

**Solution: Question 3** 



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3.4) The total rate of heat flow from the area  $\pi r^2$  of the hot surface to the drop is  $\frac{\pi r^2 \mathcal{K} \Delta T}{b}$ . We assume that this heat goes into vaporizing the drop.

Hence

$$\rho Q \ell = \frac{\pi r^2 \mathcal{K} \Delta T}{h}$$
 and using (v) we get

$$\frac{dP}{dr} = -\left(\frac{6\eta \mathcal{K}\Delta T}{\rho_{V}\ell b^{4}}\right) \cdot r \qquad (0.4 \text{ point})$$

This gives

$$P(r) = -\left(\frac{3\eta \mathcal{K}\Delta T}{\rho_{V}\ell b^{4}}\right) \cdot r^{2} + B \qquad (0.4 \text{ point})$$

where B is an arbitrary constant whose value can be found by applying the boundary condition  $P(R) = P_a$ , the atmospheric pressure.

Hence

$$B = P_{\rm a} + \left(\frac{3\eta \mathcal{K}\Delta T}{\rho_{\rm V}\ell b^4}\right) \cdot R^2 \qquad (0.4 \text{ point})$$

and

$$P(r) = P_{\rm a} + \left(\frac{3\eta \mathcal{K}\Delta T}{\rho_{\rm v}\ell b^4}\right) \cdot \left(R^2 - r^2\right) \qquad (0.8 \text{ point})$$

3.5) The net force due to pressure is in the upward direction and of magnitude

$$f = \int_{r=0}^{R} \left[ P(r) - P_{a} \right] 2\pi r dr = \frac{3\pi \eta \mathcal{K} \Delta T R^{4}}{2\rho_{V} \ell b^{4}} \qquad \dots \dots \dots (ix)$$
 (1.0 point)

The weight of the drop is  $\frac{2}{3}\pi R^3 \rho_0 g$ , where  $\rho_0$  is the density of liquid.

$$\therefore \frac{2}{3}\pi R^3 \rho_0 g = \frac{3\pi\eta \mathcal{K}\Delta T R^4}{2\rho_V \ell b^4}$$

$$b = \left(\frac{9\eta \mathcal{K}R\Delta T}{4\rho_0\rho_V \ell g}\right)^{\frac{1}{4}} \qquad \dots (x)$$



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Note that

$$\frac{3\eta\mathcal{K}\Delta T}{\rho_{\mathcal{V}}\ell b^4} = \frac{4}{3}\frac{\rho_0 g}{R} \qquad \dots \dots \dots \dots (xi)$$
 (1.0 point)

3.6) Use equations (xi) and (viii) to obtain

$$P(r) = P_{a} + \left(\frac{4}{3}\frac{\rho_{0}g}{R}\right) \cdot \left(R^{2} - r^{2}\right) \qquad ..... (xii)$$

$$\frac{d}{dr}P(r) = -\left(\frac{8}{3}\frac{\rho_{0}g}{R}\right) \cdot r \qquad ..... (xiii)$$
(0.8 point)

Then use (v) to calculate the total mass-rate of vaporization  $Q\rho_{V}$  at r=R:

$$Q\rho_{V} = \left(\frac{2\pi b^{3}R}{12\eta}\right)\left(\frac{8}{3}\frac{\rho_{0}g}{R}\right)R\rho_{V} = \left(\frac{4\pi\rho_{V}\rho_{0}gR}{9\eta}\right)b^{3}$$

$$= \left(\frac{4\pi\rho_{V}\rho_{0}gR}{9\eta}\right)\left(\frac{9\eta\mathcal{K}R\Delta T}{4\rho_{0}\rho_{V}\ell g}\right)^{\frac{3}{4}}$$

$$= \left(\frac{4\pi^{4}\mathcal{K}^{3}\rho_{V}\rho_{0}g\left(\Delta T\right)^{3}}{9\eta\ell^{3}}\right)^{\frac{1}{4}}\cdot R^{\frac{7}{4}} = \beta R^{\frac{7}{4}} \dots (xiv) \quad (1.2 \text{ points})$$

3.7) The life-time  $(\tau)$  of the drop, is to be found from

$$\frac{d}{dt} \left( \frac{2}{3} \pi R^3 \rho_0 \right) = -Q \rho_V = -\beta R^{\frac{7}{4}}$$

$$R^{\frac{1}{4}} \frac{d}{dt} R = -\frac{\beta}{2\pi \rho_0}$$

$$\int_{R}^{0} R^{\frac{1}{4}} dR = -\int_{0}^{\tau} \frac{\beta}{2\pi \rho_0} dt$$
(1.0 point)

$$\tau = \frac{8\pi\rho_0}{5\beta} R^{\frac{5}{4}} = \frac{8}{5} \left( \frac{9\eta\rho_0^3 \ell^3}{4\kappa^3 \rho_V g (\Delta T)^3} \right)^{\frac{1}{4}} \cdot R^{\frac{5}{4}}$$
 (1.0 point)

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